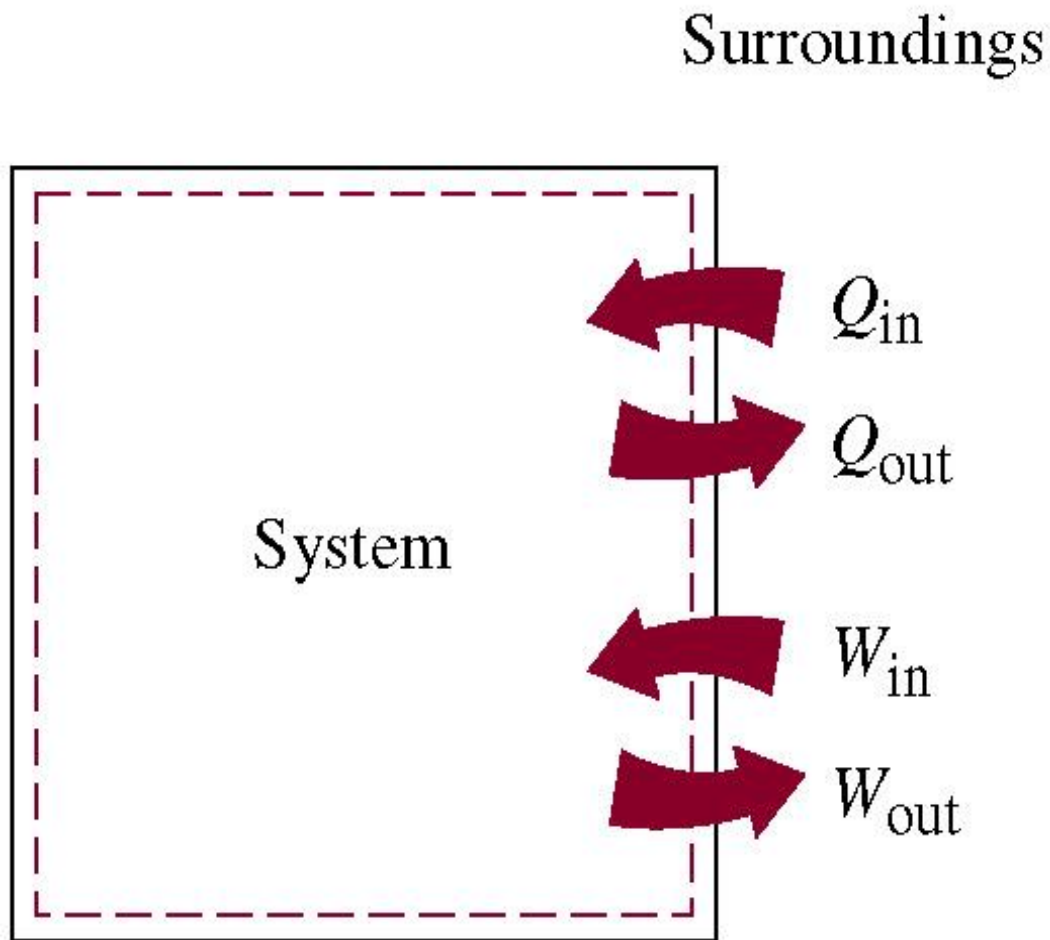


**The First Law of  
Thermodynamics:  
*Closed Systems***

## Closed system

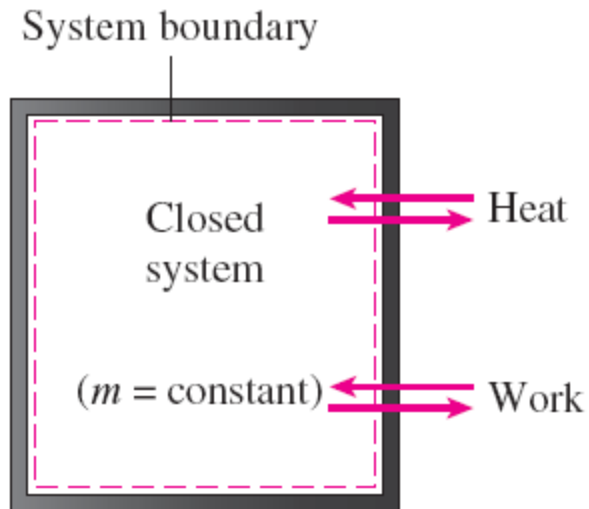
Energy can cross the boundary of a closed system in two forms: Heat and work

**FIGURE 3-1**  
Specifying the directions of heat and work.



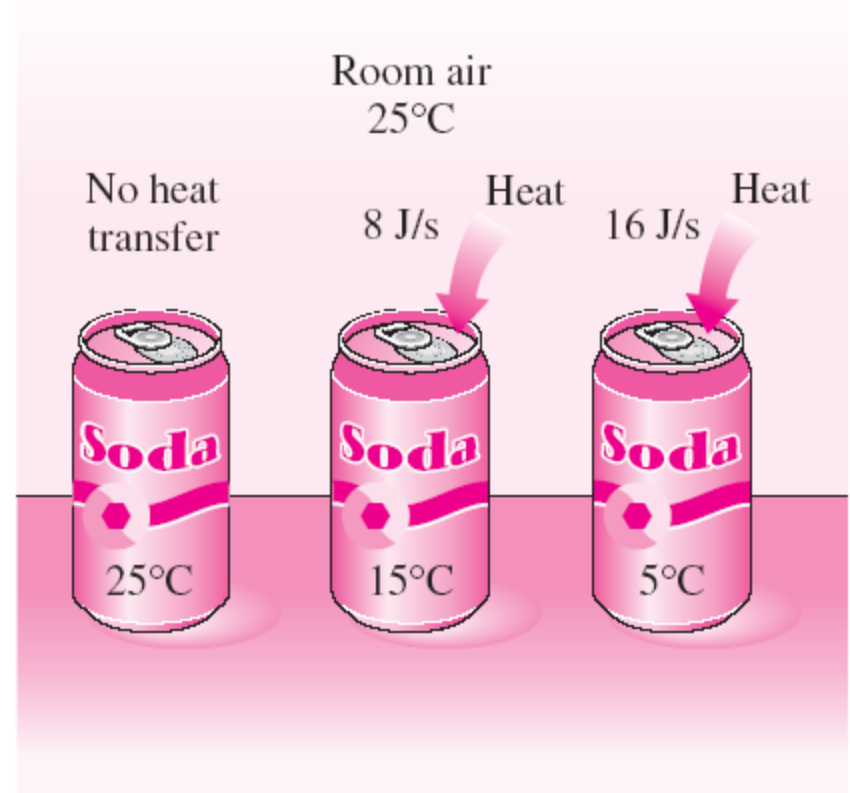
# ENERGY TRANSFER BY HEAT

**Heat:** The form of energy that is transferred between two systems (or a system and its surroundings) by virtue of a temperature difference.



**FIGURE 2-13**

Energy can cross the boundaries of a closed system in the form of heat and work.



**FIGURE 2-14**

Temperature difference is the driving force for heat transfer. The larger the temperature difference, the higher is the rate of heat transfer.

$$q = \frac{Q}{m} \quad (\text{kJ/kg})$$

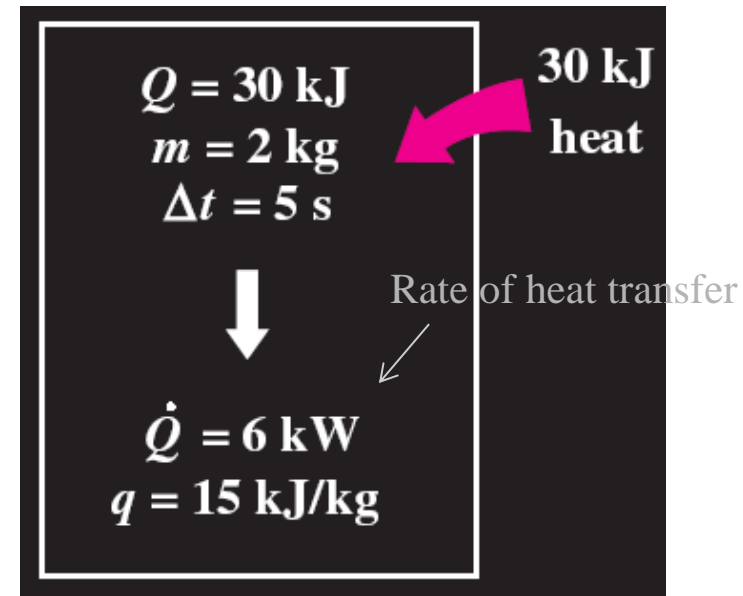
Heat transfer per unit mass

$$Q = \dot{Q} \Delta t \quad (\text{kJ})$$

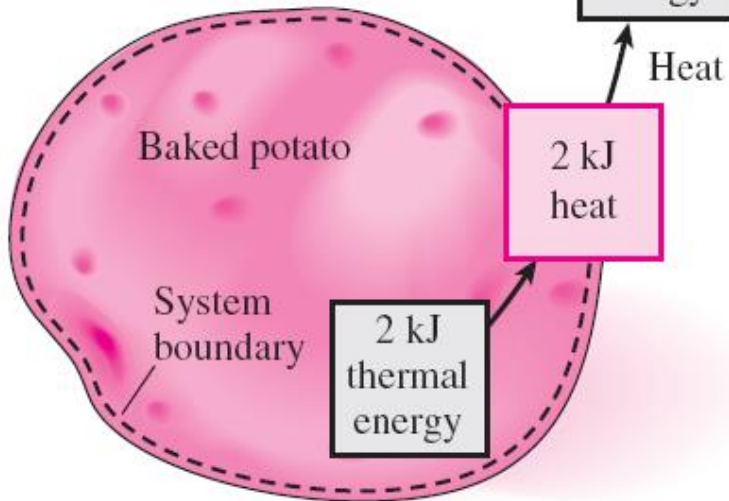
Amount of heat transfer when heat transfer rate is constant

$$Q = \int_{t_1}^{t_2} \dot{Q} dt \quad (\text{kJ})$$

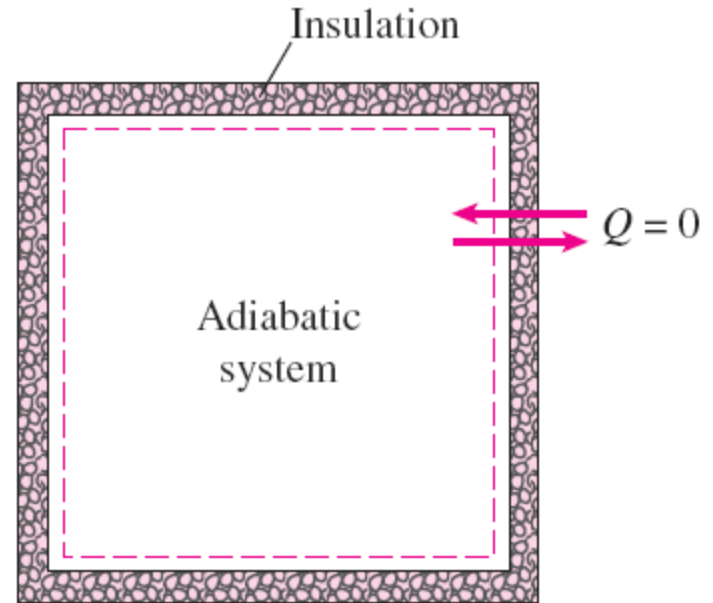
Amount of heat transfer when heat transfer rate changes with time



Surrounding air



Energy is recognized as heat transfer only as it crosses the system boundary.

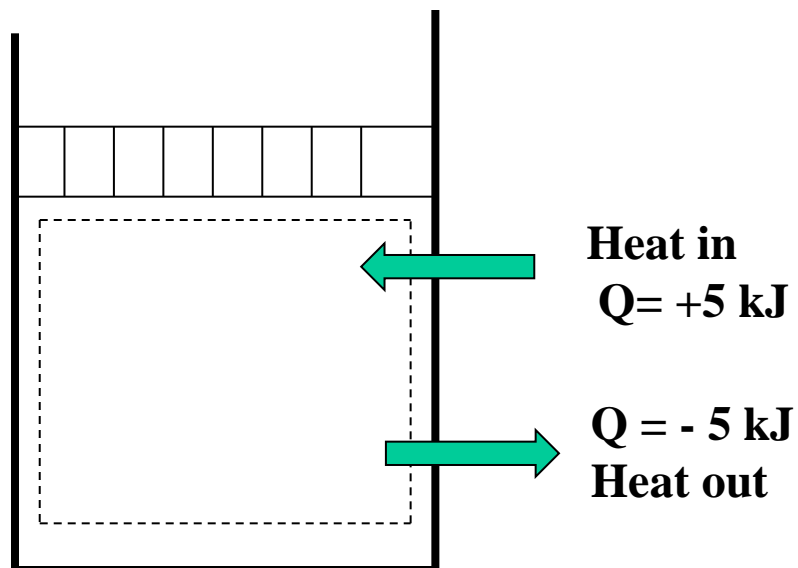


During an adiabatic process, a system exchanges no heat with its surroundings.

## Sign Convention for Heat

(+) ve if to the system

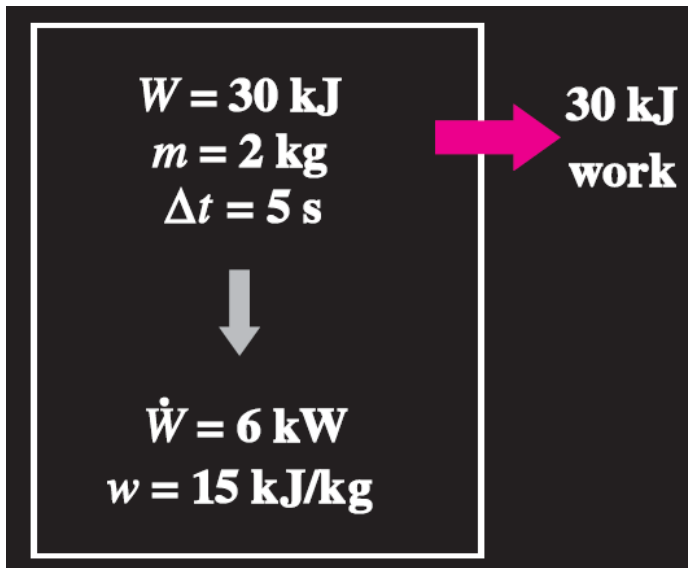
(-) ve if from the system



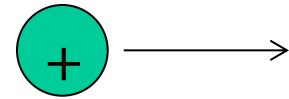
# ENERGY TRANSFER BY WORK

- **Work:** The energy transfer associated with a force acting through a distance.
- Or an energy interaction which is not caused by a temperature difference between a system and its surroundings
  - **A rising piston, a rotating shaft, and an electric wire crossing the system boundaries** are all associated with work interactions

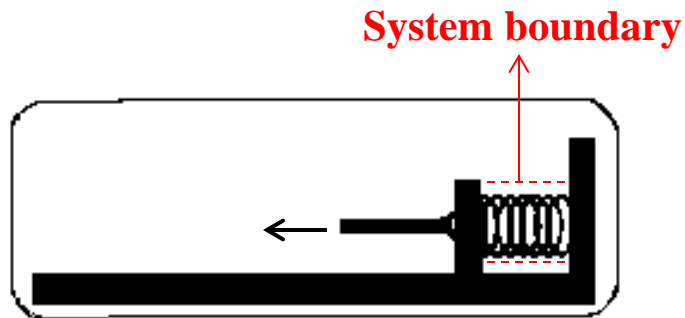
$$w = \frac{W}{m} \quad (\text{kJ/kg}) \quad \text{Work done per unit mass}$$



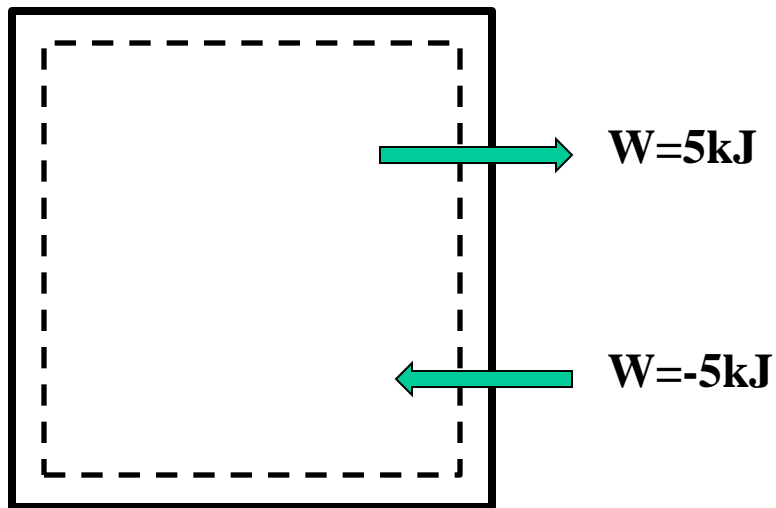
Power is the work done per unit time (kW)



Moving a positive charge from one place to another requires work



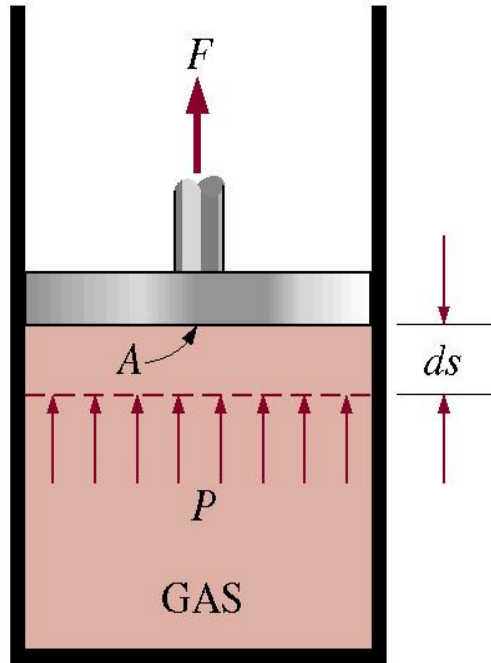
A spring is doing work on the surroundings



**Sign Convention of Work**

**(+)ve if work done by a system**

**(-)ve if work done on a system**



**Moving boundary work ( $P dV$  work):**  
The expansion and compression work in a piston-cylinder device.

$$\delta W_b = F ds = PA ds = P dV$$

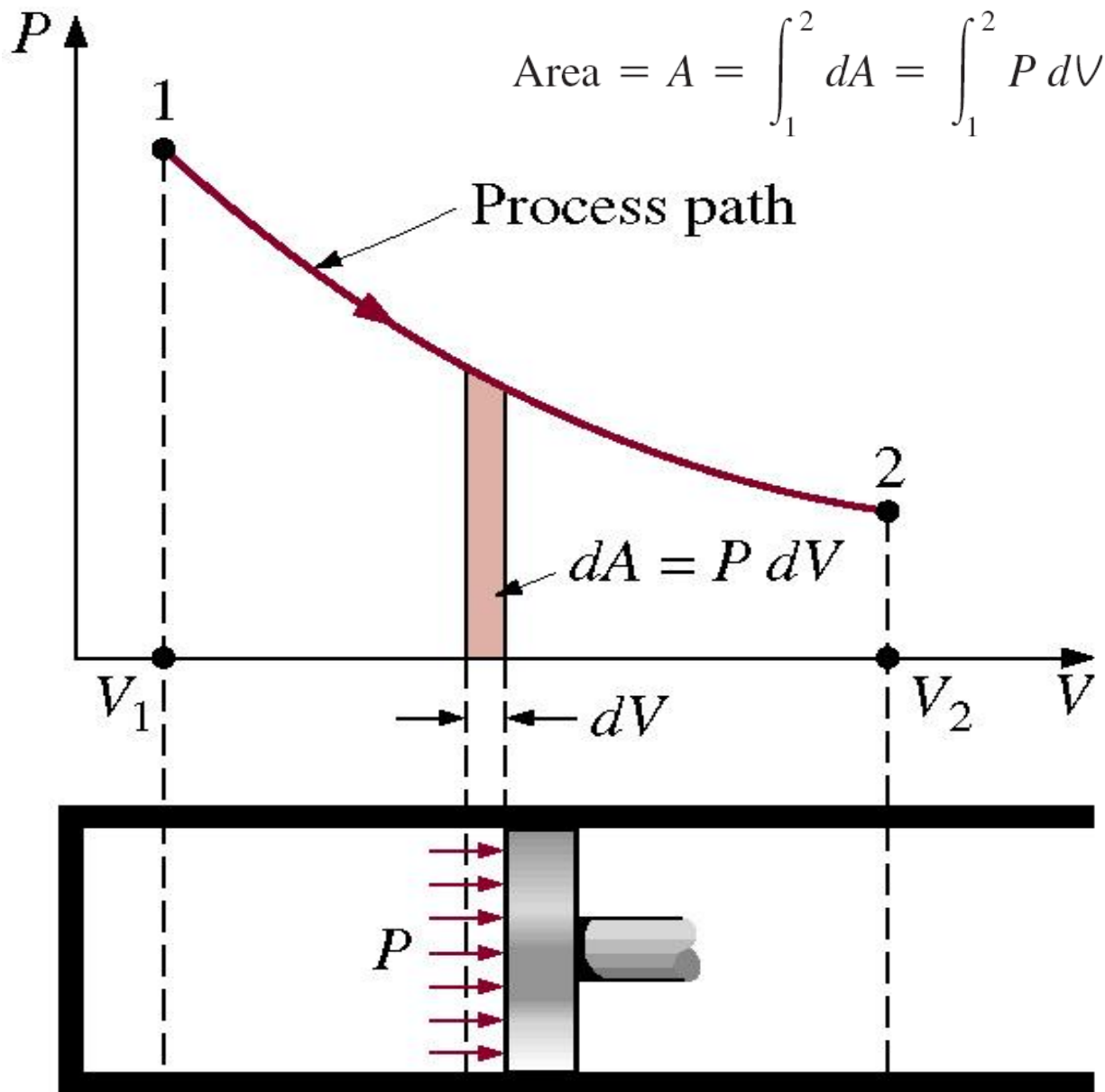
$$W_b = \int_1^2 P dV \quad (\text{kJ})$$

**FIGURE 3-2**

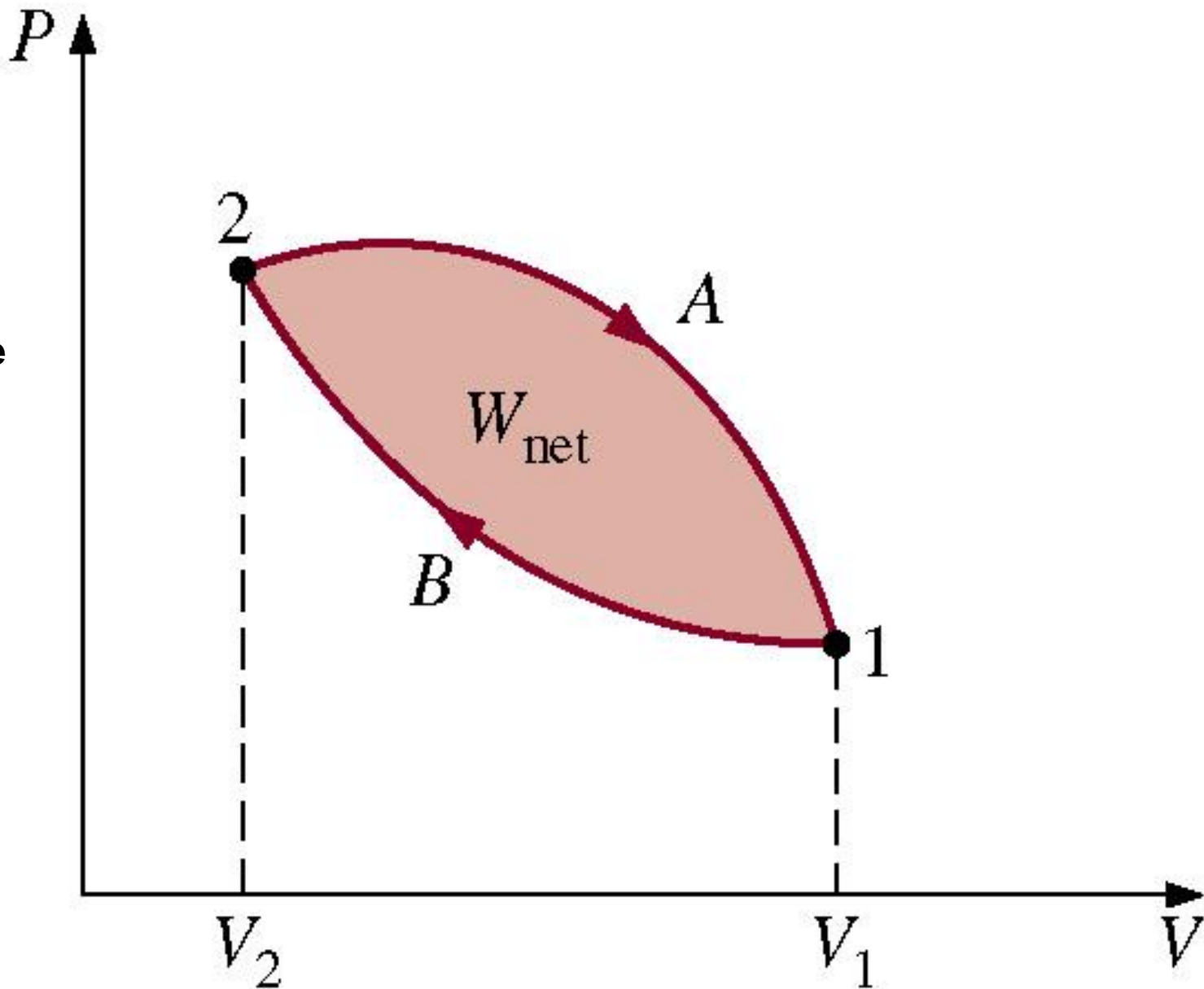
A gas does a differential amount of work  $dW_b$  as it forces the piston to move by a differential amount  $ds$ .



The area under the process curve on a  $P$ - $V$  diagram represents the boundary work.



The net work done during a cycle is the difference between the work done by the system and the work done on the system.



First Law of Thermodynamics or the Conservation of energy Principle:

{ Net energy transfer  
to (or from) the system  
As heat and work } = { Net increase (or decrease)  
In the total energy  
of the system }

$$Q - W = \Delta E$$

$$Q_{\text{net,in}} - W_{\text{net,out}} = \Delta E_{\text{system}} \quad \text{or} \quad Q - W = \Delta E$$

**(Remember from chapter 1:  $\Delta E = \Delta U + \Delta KE + \Delta PE$  )**

$$Q - W = \Delta U + \Delta KE + \Delta PE \quad (\text{kJ})$$

where  $\Delta U = m(\mathbf{u}_2 - \mathbf{u}_1)$

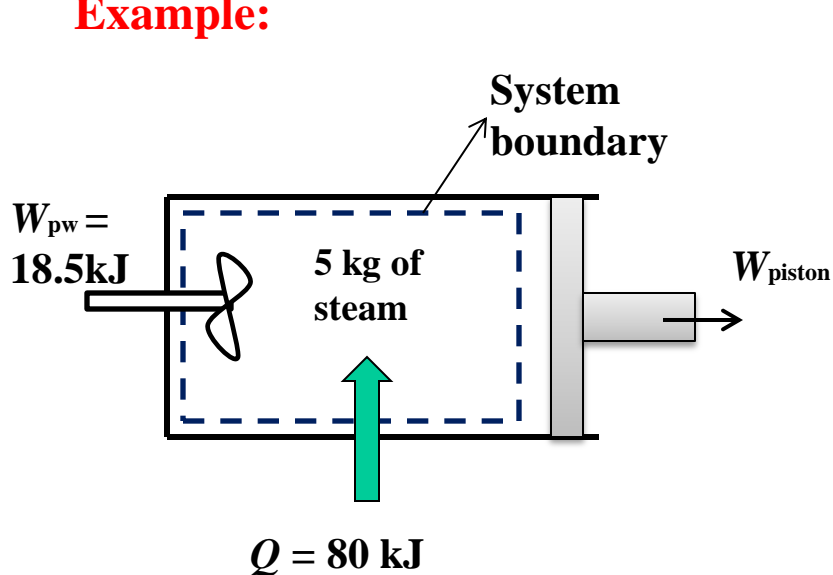
$$\Delta KE = 1/2 m(V_2^2 - V_1^2)$$

$$\Delta PE = mg(Z_2 - Z_1)$$

Most closed systems  
encountered in  
practice are stationary  
i.e.  $\Delta PE = 0$   $\Delta KE = 0$

$$Q - W = \Delta U$$

**Example:**



$$Q - W = \Delta U + \overset{0}{\cancel{\Delta KE}} + \overset{0}{\cancel{\Delta PE}}$$

$$\rightarrow \Delta U = m(u_2 - u_1)$$

$$\rightarrow W = W_{pw} + W_{piston}$$

$$Q - (W_{pw} + W_{piston}) = m(u_2 - u_1)$$

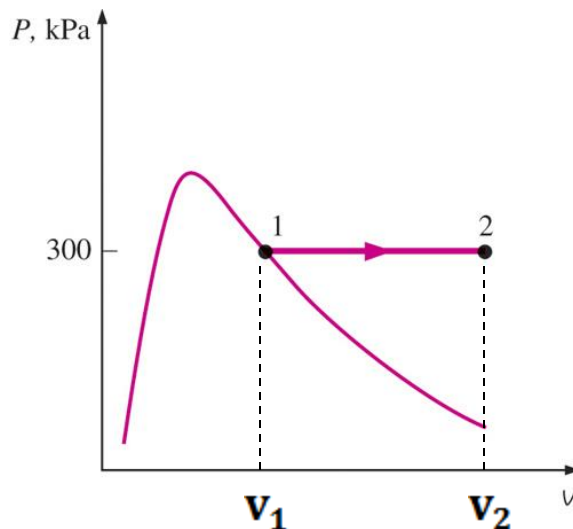
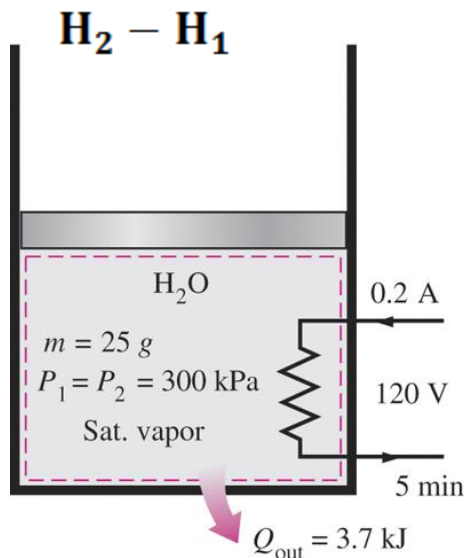
$$u_1 = 2709.9 \text{ kJ/kg}$$

$$u_2 = 2659.6 \text{ kJ/kg}$$

$$(+80 \text{ kJ}) - ((-18.5 \text{ kJ}) + W_{piston}) = (5 \text{ kg})(2659.6 - 2709.9) \text{ kJ/kg}$$

$$\rightarrow W_{piston} = 350 \text{ kJ}$$

**Example:** constant-pressure process, initially saturated water vapor.  $T_2 = ?$



$$w_b = P(v_2 - v_1)$$

$$W_b = P(V_2 - V_1)$$

$$\underbrace{E_{\text{in}} - E_{\text{out}}}_{\text{Net energy transfer by heat, work, and mass}} = \underbrace{\Delta E_{\text{system}}}_{\text{Change in internal, kinetic, potential, etc., energies}}$$

$$Q - W = \Delta U + \cancel{\Delta KE}^0 + \cancel{\Delta PE}^0$$

$$Q - W_{\text{other}} - W_b = U_2 - U_1$$

$$Q - W_{\text{other}} - P_0(V_2 - V_1) = U_2 - U_1$$

$$Q - W_{\text{other}} = (U_2 + P_2V_2) - (U_1 + P_1V_1)$$

$$H = U + PV$$

$$Q - W_{\text{other}} = H_2 - H_1$$

$$Q - W_{\text{el}} = m(h_2 - h_1) =$$

$$-3.7 \text{ kJ} - (-7.2 \text{ kJ}) = 0.025 \text{ kg} (h_2 - 2725.3 \text{ kJ/kg})$$

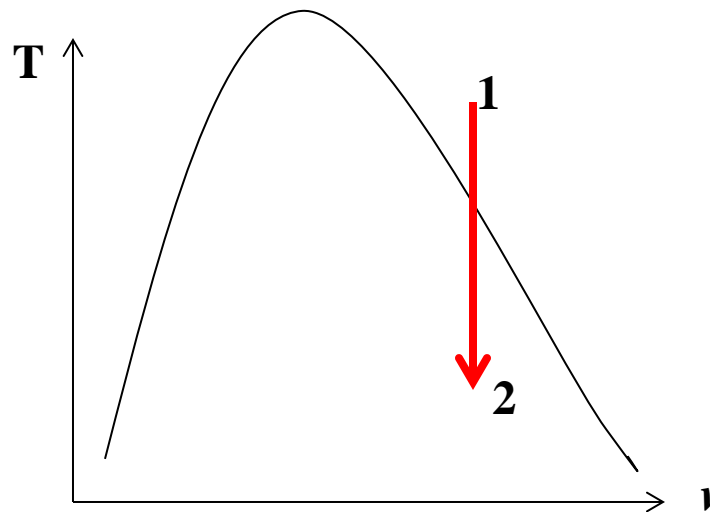
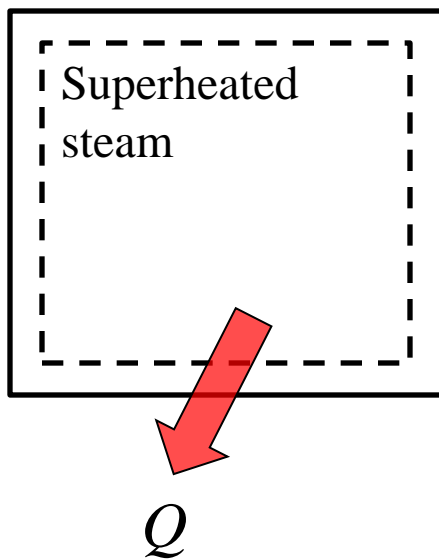
$$h_2 = 2865.3 \text{ kJ/kg}$$

$$\left. \begin{array}{l} P_2 = 300 \text{ kPa} \\ h_2 = 2865.3 \end{array} \right\}$$

$$T_2 = 200^\circ\text{C} \quad \text{Table A-6}$$

**Note:** for constant pressure case:  $Q - W_{\text{other}} = \Delta H$  and  $W = W_{\text{boundary}} + W_{\text{other}}$

**Example: constant volume**

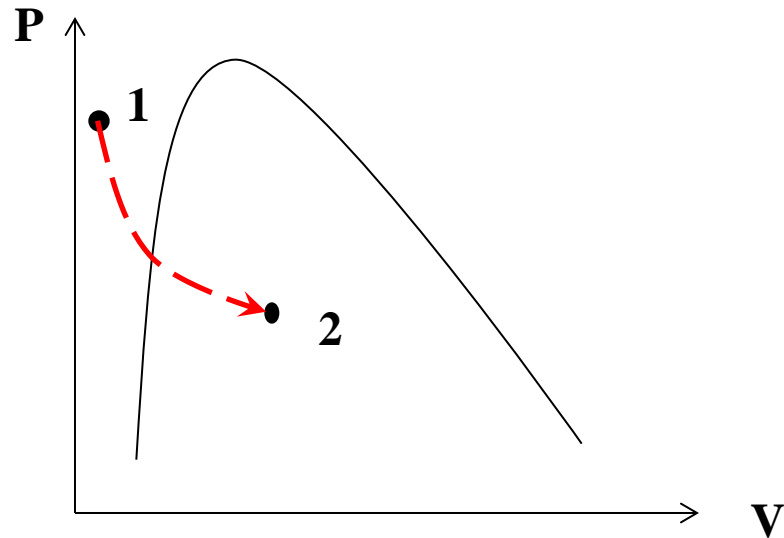
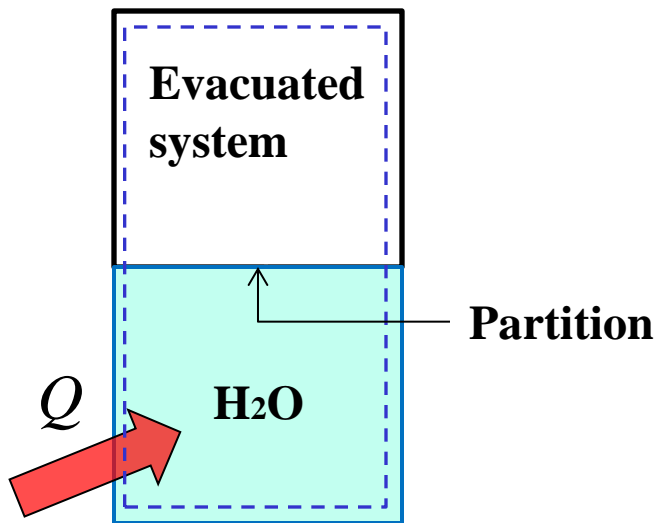


$$Q - \cancel{W} = \Delta U + \cancel{\Delta KE} + \cancel{\Delta PE}$$

$$Q = m(u_2 - u_1)$$

**Note: for constant volume case:**  $Q - W_{other} = \Delta U + \Delta KE + \Delta PE$

**Example:** changing volume and pressure



$$Q - \overset{0}{\uparrow} \cancel{W} = \Delta U + \overset{0}{\uparrow} \cancel{\Delta KE} + \overset{0}{\uparrow} \cancel{\Delta PE}$$

$$Q = m(u_2 - u_1)$$

note:  $u_1 \approx u_{f@T_{sat}}$

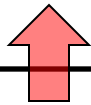
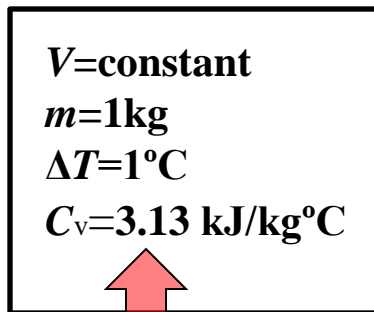
$$u_2 = u_f + x_2 u_{fg}$$



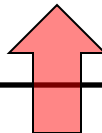
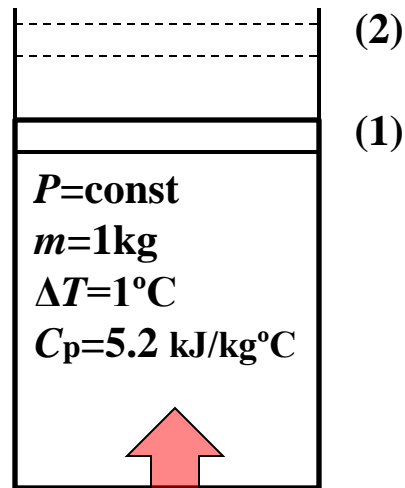
## Specific Heats

- The energy required to raise the temperature of a unit of a substance by one degree.
- $C_v$  : specific heat at constant volume
- $C_p$  : specific heat at constant pressure

**Helium gas:**



**3.13kJ**



**5.2kJ**

$$C_p > C_v$$

Because at constant pressure, the energy required for expansion work must also be supplied to system.

**First law for constant volume:**

$$(\mathbf{w}_b = \mathbf{0}) \rightarrow \delta\mathbf{q} - \delta\mathbf{w}_{\text{other}} = \mathbf{d}\mathbf{u}$$

$\underbrace{\hspace{10em}}$   
 $C_v dT$

$$\rightarrow \mathbf{d}\mathbf{u} = C_v dT \text{ or } C_v = \left(\frac{\partial \mathbf{u}}{\partial T}\right)_v$$

**First law for constant pressure:**

$$(\mathbf{w}_b \neq \mathbf{0}) \rightarrow \delta\mathbf{q} - \delta\mathbf{w}_{\text{other}} = \mathbf{d}\mathbf{h}$$

$\underbrace{\hspace{10em}}$   
 $C_p dT$

$$\rightarrow \mathbf{d}\mathbf{h} = C_p dT \text{ or } C_p = \left(\frac{\partial \mathbf{h}}{\partial T}\right)_h$$

**Ideal Gases:**

$$Pv = RT$$

**Joule demonstrated that for ideal gases  $\rightarrow u=u(T) \rightarrow C_v=C_v(T)$**

$$\left. \begin{array}{l} h = u + Pv \\ Pv = RT \end{array} \right\} h = u + RT$$

**Since  $R$  is constant and  $u=u(T) \rightarrow h=h(T) \rightarrow C_p=C_p(T)$**

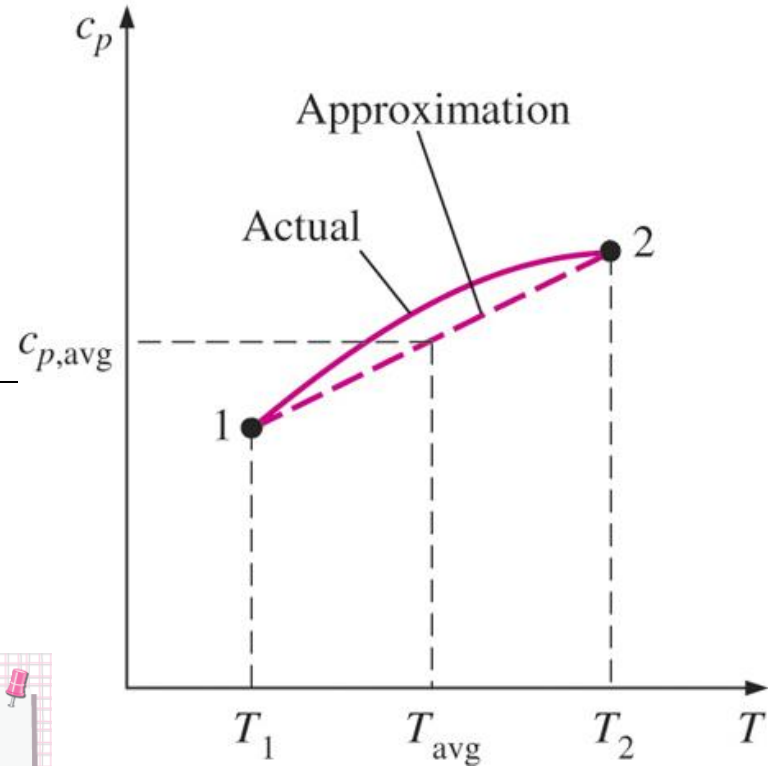
$$du = C_v dT \quad \text{and} \quad dh = C_p dT$$

### Three ways of calculating $\Delta u$ and $\Delta h$

$$\Delta h = h_2 - h_1 \quad \leftarrow \text{from tables}$$

$$\Delta h = \int_1^2 c_p(T) dT$$

$$\Delta h \cong c_{p,avg} \Delta T$$



Similarly:

$$\Delta u = u_2 - u_1 \quad (\text{table})$$

$$\Delta u = \int_1^2 c_v(T) dT$$

$$\Delta u \cong c_{v,avg} \Delta T$$

$$\Delta u = u_2 - u_1 = \int_1^2 c_v(T) dT$$

$$\Delta h = h_2 - h_1 = \int_1^2 c_p(T) dT$$

$$h = \bar{u} + RT, \xrightarrow{\text{differentiate}} dh = du + R dT$$

$$\longrightarrow c_p dT = c_v dT + R dT$$

$$\div dT \longrightarrow c_p = c_v + R \quad (\text{kJ/kg} \cdot \text{K})$$

$$\text{On a molar basis} \longrightarrow \bar{c}_p = \bar{c}_v + R_u \quad (\text{kJ/kmol} \cdot \text{K})$$

$$\text{Specific heat ratio} \quad k = \frac{c_p}{c_v}$$

## Solids and Liquids:

Can be approximated as incompressible:  $c_p \cong c_v = c$

Again, specific heats depend on temperature only.

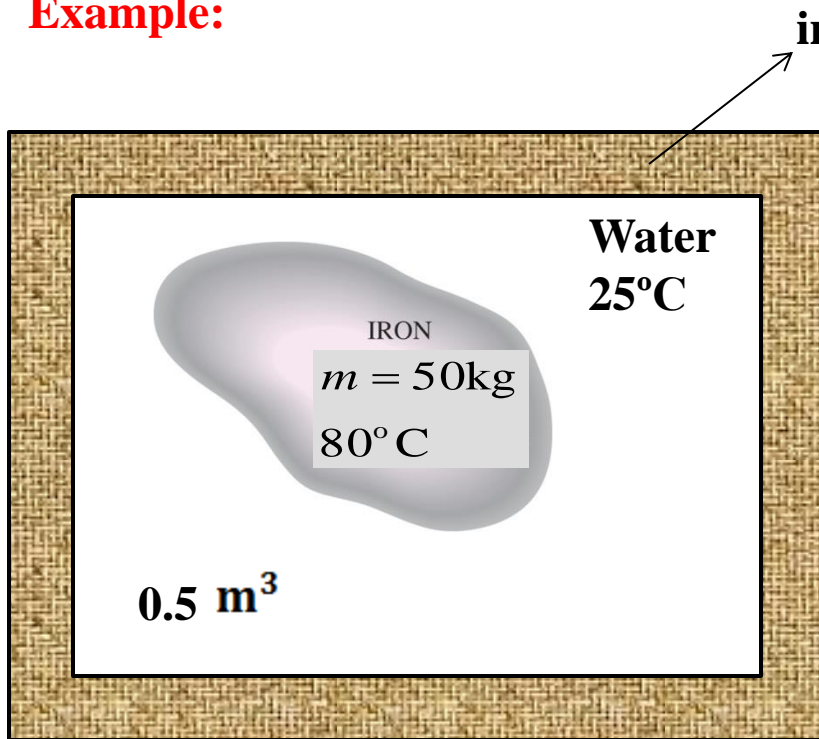
$$du = C_v dT = C(T) dT$$

The change in internal energy between states 1 and 2:

$$\Delta u = u_2 - u_1 = \int_1^2 c(T) dT$$

$$\Delta u = c_{avg} (T_2 - T_1)$$

**Example:**



$$Q-W=\Delta U \text{ or } \Delta U=0$$

$$\Delta U = \Delta U_{iron} + \Delta U_{water} = 0$$

$$[mC(T_2 - T_1)]_{iron} + [mC(T_2 - T_1)]_{water} = 0$$

$$m_{water} = \frac{V}{v_{25\text{ C}}} = \frac{0.5\text{ m}^3}{0.001\text{ m}^3/\text{kg}} = 500\text{kg}$$

**Specific heats are determined from table A-3.**

$$50\text{kg}(0.45\text{kJ}/\text{kg}^\circ\text{C})(T_2 - 80^\circ\text{C}) + 500\text{kg}(4.18\text{kJ}/\text{kg}^\circ\text{C})(T_2 - 25^\circ\text{C}) = 0$$

$$T_2 = 25.6^\circ\text{C}$$

## Example 1 – Class Work

- **Radon** gas initially at 65 kPa, 200°C is **to be heated in a closed , rigid container** until it is at 400°C. The mass of the radon is 0.393 kg.
- A table of properties shows that at 200°C, the internal energy of radon is 26.6 kJ/kg; at 400°C it is 37.8 kJ/kg.
- Determine the amount of heat required.
- Determine the final pressure

*(Draw a simple diagram and put the information on it)*



## Example 2

**Air** at a temperature of  $500^{\circ}\text{C}$  is **compressed** in a piston-cylinder arrangement at a **constant pressure** of  $1.2\text{ MPa}$  from a volume of  $2\text{ m}^3$  to a volume of  $0.4\text{ m}^3$ . if the internal energy decrease is  $4820\text{ kJ}$ , find

- the work done during the reversible compression
- The heat transferred
- The change of enthalpy
- The average specific heat at constant pressure.

$$\text{a) } W_{1-2} = P(V_2 - V_1) = 1.2 \times 10^3 \text{ kPa} [(0.4 - 2) \text{ m}^3] = -1920 \text{ kJ}$$

$$\text{b) } Q_{1-2} - W_{1-2} = U_2 - U_1 \rightarrow Q_{1-2} - (-1920 \text{ kJ}) = -4820 \text{ kJ} \rightarrow Q_{1-2} = -6740 \text{ kJ}$$

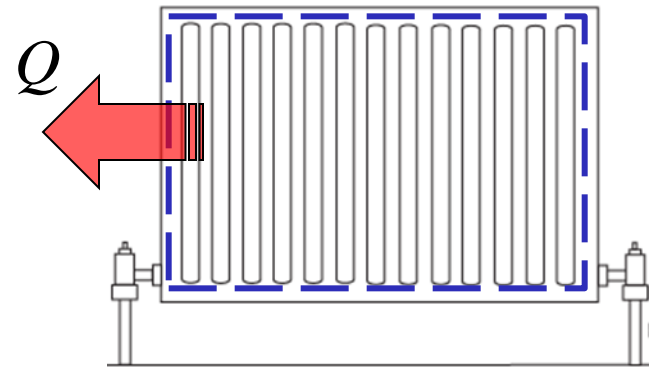
### Example 3

The radiator of a steam heating system is filled with superheated vapor. The volume of the radiator is 15 L and the inlet and outlet valves are closed. The pressure inside the radiator drops from 200 kPa to 100 kPa while dissipating heat into a room. If the initial temperature of the steam is 200°C determine the heat transferred to the room.

$$Q - W = \Delta U$$

$$Q = m(u_2 - u_1) = \frac{V}{v}(u_2 - u_1)$$

$$Q = \frac{15 \times 10^{-3} \text{ m}^3}{1.0803 \text{ m}^3/\text{kg}} (u_2 - 2654.4 \text{ kJ/kg})$$



In order to find  $u_2$  we need to find the quality at state 2

$$\rightarrow x = \frac{v - v_f}{v_{fg}} \quad \text{then use} \quad u_2 = u_f + xu_{fg}$$